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Citation for final published version:

Benzi, Roberto, Ching, Emily S. C. and De Angelis, Elisabetta ORCID: <https://orcid.org/0000-0002-9183-2413> 2016. Turbulent Rayleigh-Bénard convection with polymers: Understanding how heat flux is modified. Physical Review E 94 (6) , 063110. 10.1103/PhysRevE.94.063110 file

Publishers page: <http://dx.doi.org/10.1103/PhysRevE.94.063110>
<<http://dx.doi.org/10.1103/PhysRevE.94.063110>>

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(Received 10 October 2016; published 21 December 2016)

We study how polymers affect the heat flux in turbulent Rayleigh-Bénard convection at moderate Rayleigh numbers using direct numerical simulations with polymers of different relaxation times. We find that heat flux is enhanced by polymers and the amount of heat enhancement first increases and then decreases with the Weissenberg number, which is the ratio of the polymer relaxation time to the typical time scale of the flow. We show that this nonmonotonic behavior of the heat flux enhancement is the combined effect of the decrease in the viscous energy dissipation rate due to the viscosity of the Newtonian fluid and the increase in the energy dissipation rate due to polymers when Weissenberg number is increased. We explain why the viscous energy dissipation rate decreases with the Weissenberg number. Then by carrying out a generalized boundary layer analysis supplemented by a space-dependent effective viscosity from the numerical simulations, we provide a theoretical understanding of the change of the heat flux when the viscous energy dissipation rate is held constant. Our analysis thus provides a physical way to understand the numerical results.

DOI: [10.1103/PhysRevE.94.063110](https://doi.org/10.1103/PhysRevE.94.063110)**I. INTRODUCTION**

It is well known that adding polymers to turbulent wall-bounded flows can significantly reduce the friction drag or, equivalently, increase the mass transport. The phenomenon of turbulent drag reduction by polymers has been extensively studied since its discovery by Toms in 1948 [1]. Compared to drag reduction, the effect of polymers on the heat transport in turbulent thermal convection is much less explored and has been the focus of several recent studies [2–5]. Rayleigh-Bénard (RB) convection [6–9] is a paradigm system to study turbulent thermal convection. In the RB system, a fluid is constrained between two horizontal plates that are heated from below and cooled from above, and the system is controlled by two parameters: the Rayleigh number, $Ra = \alpha g \Delta T H^3 / (\kappa \nu_s)$, which measures the thermal forcing due to the temperature difference ΔT between the two plates, and the Prandtl number, $Pr = \nu_s / \kappa$, which is the ratio between the kinematic viscosity ν_s and the thermal diffusivity κ of the fluid. In addition, α is the isobaric volume expansion coefficient of the fluid, g is the acceleration due to gravity, and H is the vertical distance between the top and bottom plates. In turbulent RB convection, there are distinct flow regions, namely viscous boundary layers near all rigid walls and two thermal boundary layers, one above the bottom plate and one below the top plate, and an approximately homogeneous bulk flow in the central region of the convection cell.

The bulk flow of turbulent RB convection without the boundary layers is believed [10] to be a good approximation of the ultimate regime [11] at large Ra . To study the effect of polymers in this case, we have performed direct numerical simulations (DNS) of homogeneous turbulent thermal convection without boundaries using periodic boundary conditions [2] and found that polymers enhance heat transport. A similar heat enhancement by polymers has been found in Rayleigh-Taylor turbulence [4]. At variance with these results, experiments on turbulent RB convection of water at moderate Ra [3] reveal that polymers reduce heat transport and the

amount of reduction increases with polymer concentration. This reduction of heat transport by polymers at moderate Ra has also been found in a later experimental study [5]. To account for these experimental findings, some of us [12] have generalized the classical boundary layer theory [13–15] to study heat transport by boundary layer flow with polymers using the Oldroyd-B model [16], in which polymer chains can be stretched indefinitely without a limit. We recall that the classical boundary layer theory was developed for steady-state forced convection above a semi-infinite weakly heated plate [17,18] and has been shown [7,19] to provide basic understanding of the physics of heat transport in fluctuating boundary layers in turbulent RB convection at moderate Ra . On the other hand, experiments using convection cell with rough top and bottom plates indicated that heat flux is enhanced by polymers when the concentration of polymers is not too small [15,20]. It is believed that the pyramidal structures of the rough plates perturb the boundary layers and make the flow resembling that of the bulk flow even at moderate Ra .

Our work in Ref. [12] and its extension to finitely extensible polymers [21] shows that polymer stretching gives rise to a space-dependent effective viscosity in boundary layer flow. For the Oldroyd-B polymers and for polymers with large finite extensibility, the effective viscosity vanishes quickly as one moves away from the plate and is nonzero only within a region very close to the plate. In both cases, a reduction in heat transport is found and the amount of heat reduction increases with polymer concentration, in agreement with the experimental observations in Ref. [3]. It is thus reasonable to assume that the specific details of polymer stretching determine heat transport in the system.

In this paper, we investigate turbulent RB convection at moderate Ra with Oldroyd-B polymers of different relaxation times and thus different stretching behaviors. The remainder of this paper is organized as follows. In Sec. II we give a brief review of our earlier DNS study of the bulk flow without boundary layers [2] and the generalization of the classical boundary

layer theory in the presence of polymers [12]. In Sec. III we report the results of our present DNS of turbulent RB convection at moderate Ra with polymers of different relaxation times and discuss how we can use the generalized boundary layer analysis to provide a theoretical understanding of the change in heat flux due to polymers. Conclusions follow in Sec. IV.

II. REVIEW OF PREVIOUS RESULTS

In the Boussinesq approximation, the equations of motion for RB convection with polymers are

$$\frac{Du_a}{Dt} = -\nabla_a p + \nu_s \nabla^2 u_a + \nabla_b \mathcal{T}_{ab} + \alpha g(T - T_*) \delta_{az}, \quad (1)$$

$$\frac{DT}{Dt} = \kappa \nabla^2 T, \quad (2)$$

where $D/Dt \equiv \partial_t + \vec{u} \cdot \vec{\nabla}$ is the material derivative, \vec{u} is the velocity field with components u_a , $a = x, y, z$, with x and y along the horizontal directions and z along the vertical direction, p is the pressure, and T is the temperature field with T_* being the mean temperature averaged over time and the whole system. We have used the repeated indices summation convention and for simplicity the density of the fluid is taken to be 1. The polymeric stress tensor \mathcal{T}_{ab} depends on how much the polymer chains are stretched and is a function of the polymer conformation tensor R_{ab} . Let \vec{d} be the end-to-end distance vector of a polymer chain, and R_{ab} is the ensemble average of $d_a d_b$ normalized by the equilibrium value of the ensemble average of $d_a^2/3$. For Oldroyd-B polymers,

$$\mathcal{T}_{ab}(\vec{r}, t) = \frac{\nu_p}{\tau} [R_{ab}(\vec{r}, t) - \delta_{ab}] \quad (3)$$

and the equation of motion for R_{ab} is

$$\frac{DR_{ab}}{Dt} = \partial_c u_a R_{cb} + R_{ac} \partial_c u_b - \frac{1}{\tau} (R_{ab} - \delta_{ab}). \quad (4)$$

Here ν_p is the polymer contribution to the zero-shear viscosity of the polymer solution, which increases with polymer concentration, and τ is the relaxation time of the polymers. Heat transport is measured by the dimensionless Nusselt number (Nu), which is the normalized heat flux defined by

$$\text{Nu} \equiv \frac{\langle u_z T - \kappa \partial_z T \rangle_A}{\kappa \Delta T / H}, \quad (5)$$

where $\langle \cdots \rangle_A$ denotes an average over a horizontal plane of the convection cell and time.

Equations (1)–(4) have been studied in two different limits, namely (a) large Ra with periodic boundary conditions [2,4] and (b) moderate Ra with no-slip boundary condition for velocity and isothermal boundary condition for temperature [12]. Case (a) corresponds to the ultimate regime [11] in which Nu scales as $\text{Ra}^{1/2}$. In this case, numerical simulations show an increase of Nu when polymers are added to the system. For case (b), the effect of polymers has been analyzed in the framework of the classical boundary layer theory, which has been known [7,19] to be a good approximation for moderate Ra and stable boundary layers. We will review the two cases separately in order to highlight the different physics.

In the ultimate regime, most of the energy dissipation is supposed to occur in the bulk of the system. In this case,

polymers enhance the length scale l_T of thermal plumes and the correlation of vertical velocity and temperature fluctuations, and Nu increases with the polymer relaxation time τ or equivalently, the Weissenberg number Wi, defined by

$$\text{Wi} \equiv \frac{\tau U_c}{H}, \quad (6)$$

where $U_c = \sqrt{\alpha g \Delta T H}$. More precisely, we find that $\text{Nu} \sim l_T^{3/2} \sim \text{Wi}^{3/2}$.

On the other hand, the experimental investigation of the problem at moderate Ra [3,5] reported a small but clear reduction of Nu in the presence of polymers. At low Ra, most of the energy dissipation is concentrated in the boundary layers, and therefore the numerical results reviewed above for the ultimate regime do not apply. In an attempt to understand these experimental results, some of us have generalized the classical theory for boundary-layer flow with polymers in Ref. [12]. The Prandtl-Blasius [13,14] boundary-layer equation of motion for the steady-state velocity field $u_x \hat{x} + u_z \hat{z}$ is

$$u_x \partial_x u_x + u_z \partial_z u_x = \nu_s \partial_{zz}^2 u_x. \quad (7)$$

Here x denotes the direction along the plate, z is the direction perpendicular to the plate, and $u_x \rightarrow U$ as $z \rightarrow \infty$. The mainstream velocity U plays the role of the large-scale mean flow velocity in turbulent RB convection. The crucial point about Eq. (7) is that the viscous term is balanced against the nonlinear advection term and that $\partial_z \gg \partial_x$. The latter is satisfied for flows with large Reynolds number. Introducing the stream function

$$\Psi(x, z) \equiv \sqrt{\nu_s x} U \phi(\xi) \quad (8)$$

with

$$\xi \equiv \sqrt{\frac{U}{\nu_s x}} z \quad (9)$$

such that $u_x = \partial_z \Psi$ and $u_z = -\partial_x \Psi$, we obtain the famous Blasius equation [14]

$$2\phi_{\xi\xi\xi} + \phi\phi_{\xi\xi} = 0. \quad (10)$$

Here ϕ_{ξ} denotes $\partial_{\xi} \phi$. The no-slip boundary conditions, $u_x = u_z = 0$ at the plate, and the condition $u_x \rightarrow U$ far away from the plate lead to

$$\phi(0) = \phi_{\xi}(0) = 0; \quad \phi_{\xi}(\infty) = 1. \quad (11)$$

Following the works of Prandtl [13] and Blasius [14], Pohlhausen [15] obtained also the equation for temperature field. By writing the temperature field as

$$T(x, z) = T_0 + (T_1 - T_0)\theta(\xi), \quad (12)$$

where T_1 and T_0 are respectively the temperatures at the plate and far away from the plate (or at the center of the convection cell in turbulent RB convection), $\theta(\xi)$ satisfies the equation

$$2\theta_{\xi\xi} + \text{Pr} \phi \theta_{\xi} = 0 \quad (13)$$

with the boundary conditions

$$\theta(0) = 1; \quad \theta(\infty) = 0. \quad (14)$$

In the presence of polymers described by the Oldroyd-B model, Eq. (7) is modified to [12,21]

$$u_x \partial_x u_x + u_z \partial_z u_x = \nu_s \partial_{zz}^2 u_x + \frac{\nu_p}{\tau} \partial_z (R_{xz}). \quad (15)$$

Replacing ν_s by the zero-shear viscosity $\nu_0 = \nu_p + \nu_s$ of the polymer solution in Eqs. (8) and (9), one obtains

$$-\frac{1}{2} \phi \phi_{\xi\xi} = (1 - \gamma) \phi_{\xi\xi\xi} + \frac{\gamma}{\text{Wi}_b \sqrt{\text{Re}_b}} \partial_\xi R_{xz}, \quad (16)$$

where

$$\gamma \equiv \frac{\nu_p}{\nu_s + \nu_p} \quad (17)$$

increases with the polymer concentration, and

$$\text{Re}_b = \frac{UH}{\nu_0}, \quad (18)$$

$$\text{Wi}_b = \frac{\tau U}{H} \quad (19)$$

are respectively the Reynolds and Weissenberg numbers of the boundary layer flow. To obtain Eq. (16), we have used the approximation of replacing x by the length H of the (large) plate in the final equation, and this approximation is consistent with the boundary layer description, which is meant to be applicable for x being large. The final step to close the problem is to express R_{xz} in terms of $\phi(\xi)$, which can be done numerically [12,21]. By writing $\nu_p R_{xz}(\xi) \equiv \tau \nu_{\text{eff}}(\xi) \partial_z u_x \approx \text{Wi}_b \sqrt{\text{Re}_b} \nu_{\text{eff}}(\xi) \phi_{\xi\xi}$ again with the approximation of replacing x by H in the last step, Eq. (16) can always be written as

$$2\partial_\xi \{ [1 + g(\xi)] \phi_{\xi\xi} \} + \phi \phi_{\xi\xi\xi} = 0, \quad (20)$$

where

$$g(\xi) \equiv \frac{\nu_{\text{eff}}(\xi)}{\nu_0} - \gamma \quad (21)$$

with $g(0) = 0$ and $g(\xi) \rightarrow 0$ as $\xi \rightarrow \infty$. The form of the temperature equation [Eq. (13)] remains unchanged, with Pr becoming ν_0/κ and $\phi(\xi)$ governed by Eq. (20) instead of the Blasius equation [Eq. (10)]. The generalization of the classical boundary layer theory to boundary-layer flow with polymers thus shows that the effect of polymer can be represented by a space-dependent effective viscosity $\nu_{\text{eff}}(\xi)$. The function $g(\xi)$ can be numerically computed and its specific profile depends on the system parameters, namely Re_b , Pr , Wi_b , and γ . For the parameters range explored in Ref. [12], $g(\xi)$ is peaked close to the boundary, and a decrease in Nu compared to the value Nu_0 for the Newtonian case with $g(\xi) = 0$ (which corresponds to a Newtonian fluid with kinematic viscosity ν_0) is observed with the amount of heat reduction increasing with γ or the polymer concentration, in qualitative agreement with the experimental observation reported in Ref. [3].

The results from the generalized Prandtl-Blasius-Pohlhausen (PBP) boundary-layer theory are interesting for two reasons. First, one can understand the role played by the viscous boundary layers which is relevant for experimental results at moderate Ra . Second, we have shown that polymer effects in the boundary layers are equivalent to a space-dependent effective viscosity. In the following, we show that the profile of the space-dependent effective viscosity is one

crucial feature for understanding the effect of polymers on heat transport in turbulent RB convection.

III. NUMERICAL SIMULATIONS

In this section, we report our present DNS of turbulent RB convection at moderate Ra with polymers of different Wi . Specifically, we integrate numerically Eqs. (1)–(4) in a three-dimensional Cartesian domain of size $8 \times 8 \times 1$ along the horizontal x and y directions with periodic boundary conditions and the vertical direction z . The discretization method is a pseudospectral one where Chebychev polynomials are used in the z direction with Fourier modes in the x and y directions. Time integration is performed with a fourth-order Runge-Kutta–Crank-Nicholson scheme. Periodic boundary conditions are imposed at the lateral planes whereas fixed-temperature and no-slip boundary conditions are used at the top and bottom plates. The DNS is performed for a Newtonian fluid of $\text{Pr} = 7$ with Oldroyd-B polymers of $\nu_p = 0.1\nu_s$ at different values of Wi using 128^2 (horizontal) \times 129 (vertical) fully dealiased modes and polynomials, which yield a spatial resolution large enough to resolve the smallest length scale of the problem. In order to accumulate reliable statistics, data over 30 eddy turnover times are collected after the initial transient is neglected. The Rayleigh number for the Newtonian fluid is $\text{Ra} = 2.07 \times 10^5$ and the Reynolds number based on U_c , H , and ν_s is given by $\text{Re} = U_c H / \nu_s = \text{Ra}^{1/2} \text{Pr}^{-1/2} = 172$.

We denote the Nusselt number for the Newtonian case without polymers by Nu_s . In Fig. 1, we show Nu/Nu_s as a function of Wi . For $\text{Wi} = 2$ we observe very little change in Nu with $\text{Nu}/\text{Nu}_s = 1.008 \approx 1$. For larger Wi , heat flux is enhanced and $\text{Nu}/\text{Nu}_s > 1$. The amount of heat flux enhancement first increases with Wi , reaching a maximum of about 20% at Wi around 10, and then decreases. The aim of this paper is to attain a theoretical understanding of this nonmonotonic heat flux enhancement by polymers. Following the discussion in Sec. II, we argue that profile of the polymer stretching plays an important role. In Fig. 2, we show the total amount of polymer stretching, measured by $\langle R_{ii} \rangle_A - 3$, as a function of the distance z from the bottom plate for the

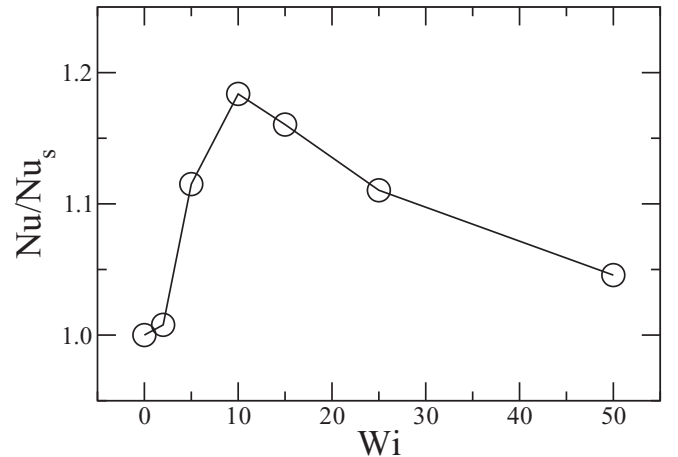


FIG. 1. Nu/Nu_s as a function of Wi . $\text{Wi} = 0$ corresponds to the Newtonian case without polymers.

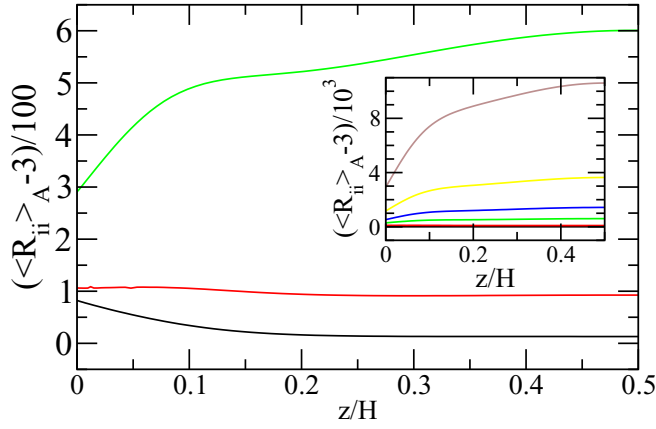


FIG. 2. $\langle R_{ii} \rangle_A - 3$ for $Wi = 2, 5$, and 10 increasing from the bottom to the top. The results for $Wi = 2$ are multiplied by a factor of 30 for clarity purpose. Inset is the plot for all the values of $Wi = 2, 5, 10, 15, 25$, and 50 increasing from the bottom to the top.

different values of Wi . For small Wi ($Wi = 2$), the amount of polymer stretching is negligible and this is consistent with the very slight change in Nu observed. The amount of polymer stretching increases significantly as Wi is increased. Moreover, we observe the interesting result that polymer stretching is extended into the bulk region of the flow and reaches a maximum at the center of the cell for large Wi ($Wi \geq 10$). We will return to this feature below.

It might appear that the monotonic increase of the amount of polymer stretching with Wi is in contradiction with the observed nonmonotonic heat flux enhancement. We will first understand why this is not so. Taking the dot product of Eq. (1) with \vec{u} and averaging over time and whole volume of the flow, we obtain

$$\alpha g \langle u_z T \rangle_V = \varepsilon_u + \varepsilon_p, \quad (22)$$

where

$$\varepsilon_u \equiv \nu_s \langle (\nabla_a u_a)^2 \rangle_V, \quad (23)$$

$$\varepsilon_p \equiv \langle -u_a \nabla_b T_{ab} \rangle_V, \quad (24)$$

and $\langle \cdots \rangle_V$ denotes an average over time and the whole volume of the convection cell. ε_u is the viscous energy dissipation rate due to the viscosity of the Newtonian fluid while ε_p is the rate of energy transfer from the fluid to the polymers which is also equal to the energy dissipation rate due to polymers as the energy transfer to the polymers is eventually dissipated as heat. Using Eq. (5), one can show that

$$Nu = \frac{\langle u_z T \rangle_V}{\kappa \Delta T / H} + 1. \quad (25)$$

Equations (22) and (25) give the exact balance between the heat flux and the sum of the two energy dissipation rates:

$$RaPr(Nu - 1) = \frac{H^4}{\kappa^3} (\varepsilon_u + \varepsilon_p). \quad (26)$$

Thus, the change in Nu is the combined effect of the changes in ε_u and ε_p with the latter change being a direct result of polymer stretching. Since the amount of polymer stretching and thus ε_p increases monotonically with Wi as shown in Fig. 2, the

observed nonmonotonic heat flux enhancement must be due to a decrease of ε_u with Wi in some range of Wi . As discussed above, the amount of polymer stretching is negligible at $Wi = 2$; thus we approximate $\varepsilon_p \approx 0$ for $Wi = 2$ and denote the value of ε_u at $Wi = 2$ by ε_{u0} . In Fig. 3 we plot $\varepsilon_u / \varepsilon_{u0}$ as a function of Wi , which shows clearly that ε_u indeed decreases with Wi .

In order to understand why ε_u decreases when Wi is increased, we recall that polymers affect a turbulent flow for scales smaller than or equal to the Lumley scale l_L , which is defined as the scale at which the time scale of energy transfer given by $l_L / \delta v(l_L)$ is equal to the polymer relaxation time. Namely,

$$\frac{l_L}{\delta v(l_L)} = \tau. \quad (27)$$

Here $\delta v(r)$ is the characteristic velocity scale of eddies of a characteristic length scale r . The effect of polymers is strongest at scales around l_L . Since $\delta v(r) \sim r^\beta$ with an exponent $0 < \beta < 1$, l_L increases with τ or Wi . When l_L approaches the system size H , polymers would interfere with the convective instability that injects energy to the system and leads to a decrease in ε_u . This is exactly what happens in our numerical simulations and a similar effect has also been observed for the ultimate regime studied in Ref. [2].

Next, we aim to provide a theoretical explanation of the change in Nu due to polymers when ε_u is held fixed. Using Eq. (26) with $Nu - 1 \approx Nu$ we obtain

$$\frac{Nu}{Nu_0} = \frac{\varepsilon_u}{\varepsilon_{u0}} + \frac{\varepsilon_p}{\varepsilon_{u0}}, \quad (28)$$

where Nu_0 is the value of Nu at $Wi = 2$ and we have used the approximation that $\varepsilon_p \approx 0$ at $Wi = 2$. If ε_u is held fixed at ε_{u0} , the relative change in heat flux, denoted by $\delta Nu / Nu_0 = Nu / Nu_0 - 1$, is given by $\varepsilon_p / \varepsilon_{u0}$. Our basic idea is that the relative change in the heat flux at a fixed viscous energy dissipation rate can be computed using the generalized PBP boundary layer theory, namely

$$\frac{Nu}{Nu_0} - \frac{\varepsilon_u}{\varepsilon_{u0}} \equiv \left(\frac{\delta Nu}{Nu_0} \right)_{\varepsilon_u \text{ fixed}} \sim \left(\frac{\delta Nu}{Nu_0} \right)_{\text{PBP}}. \quad (29)$$

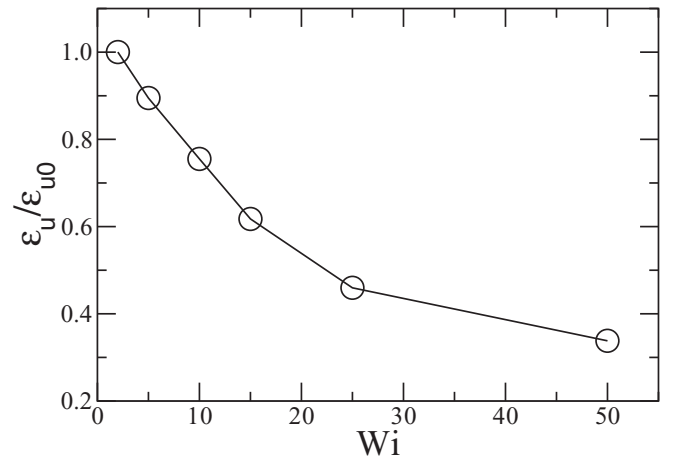


FIG. 3. $\varepsilon_u / \varepsilon_{u0}$ as a function of Wi , where ε_{u0} denotes the value of ε_u at $Wi = 2$.

As discussed above, the polymer stretching extends into the bulk region of the flow when $Wi > 2$ (see Fig. 2). This feature is in contrast to the case in laminar steady-state boundary-layer flow with polymers in which the effective viscosity vanishes quickly as one moves away from the boundary, and is nonzero only within a region very close to the boundary. This indicates that we cannot compute the effective viscosity profile due to polymer stretching self-consistently within the generalized PBP boundary layer theory. Thus we estimate $g(\xi)$ from the DNS data and use it as an external input to the generalized PBP boundary layer theory. We recall that the classical PBP boundary layer theory is in good agreement with both experimental measurements and numerical simulations obtained in turbulent RB system at moderate Ra and argue that our investigation can provide a way to theoretically understand $(\delta Nu/Nu_0)_{\varepsilon_u \text{ fixed}}$.

To obtain $g(\xi)$ from the DNS data, we note from Eq. (21) that $g(\xi)$ is related to the space-dependent effective viscosity $\nu_{\text{eff}}(\xi)$ of the polymers. We can now use our numerical simulations to get a quantitative computation of $\nu_{\text{eff}}(\xi)$. In our case, the total rate of energy change of the fluid, averaged over time and the horizontal plane of the cell, is the sum of $\varepsilon_u(z) = \nu_s \langle (\nabla_a u_a)^2 \rangle_A$ and the rate of energy dissipation due to polymers $E_p(z)$. The latter is given in terms of the polymer stretching

$$E_p(z) = \frac{1}{2} \frac{\nu_p}{\tau^2} [(R_{ii})_A(z) - 3]. \quad (30)$$

One can define a space-dependent effective viscosity $\nu_{\text{eff}}(z)$ of polymers by the relation

$$\frac{\nu_{\text{eff}}(z)}{\nu_s} = \frac{E_p(z)}{\varepsilon_u(z)} \quad (31)$$

and estimate

$$g(\xi) = \frac{\nu_{\text{eff}}(\xi) - \nu_{\text{eff}}(0)}{\nu_s}. \quad (32)$$

To relate ξ to z , we first approximate the case of $Wi = 2$ in the DNS to correspond to a Newtonian fluid with a kinematic viscosity equal to the zero-shear viscosity of the polymer solution $\nu_0 = \nu_s + \nu_p$, or equivalently with a Prandtl number $Pr_0 = \nu_0/\kappa = 7.7$. This is justified by the negligible polymer stretching at $Wi = 2$. Denote the thermal boundary layer thickness by λ_{t0} . Then we perform a calculation using the classical boundary layer theory for a Newtonian fluid with $Pr_0 = 7.7$ and obtain the corresponding $\theta'_0(0)$ and the (dimensionless) thermal boundary layer thickness $1/|\theta'_0(0)|$. Finally, ξ is related to z by $\xi|\theta'_0(0)| = z/\lambda_{t0}$.

In Fig. 4 we show $g(\xi)$ evaluated from the DNS data as a function of ξ . We see the general feature of $g(\xi)$ increases from zero and saturates to some maximum value A near the bulk. We capture this general shape by fitting the data by $g(\xi)$:

$$g(\xi) = A[1 - \exp[-(\xi/\xi_0)^\alpha]]. \quad (33)$$

The fitted values of ξ_0 are around 1 for all $Wi \geq 5$ and the fitted value of α increases from about 1 for $Wi = 5$ to 3 for $Wi = 50$. The idea is to use Eqs. (13) and (20) with this fitted form of $g(\xi)$ [Eq. (33)] to calculate $(\delta Nu/Nu_0)_{\text{PBP}}$ as a function of Wi using the generalized PBP theory. As polymer stretching extends to the bulk region and beyond the thermal boundary layers,

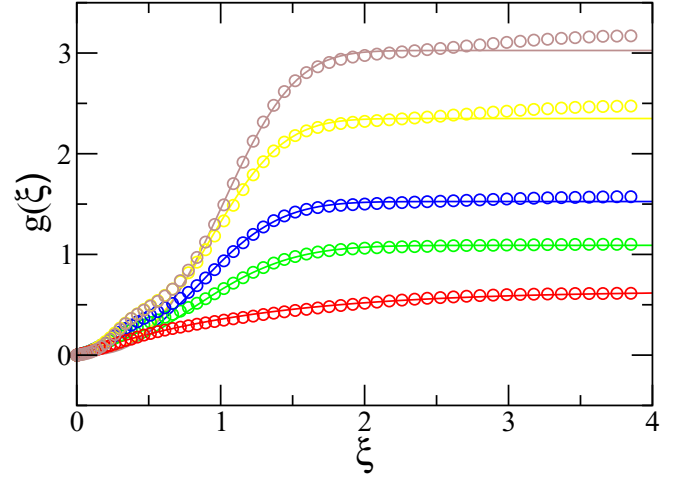


FIG. 4. The function $g(\xi)$, which is evaluated using the DNS data, measures the effective viscosity of the polymers for different Wi as a function of the dimensionless distance ξ . $Wi = 5, 10, 15, 25$, and 50 from bottom to top. The solid lines are the fits using the simplified form in Eq. (33).

heat flux enhancement is expected [21] and is indeed found. Moreover, we check that ε_u for the boundary layer flow remains approximately constant for all the effective viscosity profiles studied. We now validate the basic assumption in Eq. (29), namely

$$\left(\frac{\delta Nu}{Nu_0} \right)_{\varepsilon_u \text{ fixed}} \sim \left(\frac{\delta Nu}{Nu_0} \right)_{\text{PBP}}, \quad (34)$$

in Fig. 5 and confirm that $(\delta Nu/Nu_0)_{\varepsilon_u \text{ fixed}}$ is a simple linear function of $(\delta Nu/Nu_0)_{\text{PBP}}$. Thus the generalized PBP theory provides a theoretical way to understand the relative change in Nu due to the polymers when ε_u is held fixed. Specifically, when ε_u is held fixed, heat flux is enhanced by the polymers

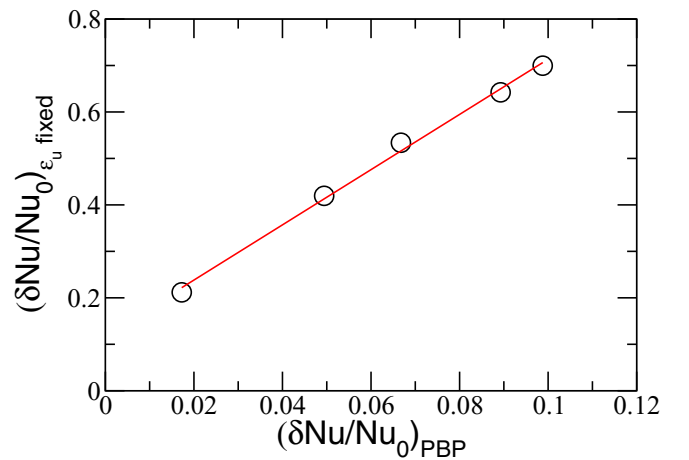


FIG. 5. Comparison of the relative change in Nu at a fixed energy dissipation rate, $(\delta Nu/Nu_0)_{\varepsilon_u \text{ fixed}}$, measured in the DNS against the theoretical value, $(\delta Nu/Nu_0)_{\text{PBP}}$, obtained using the generalized PBP boundary layer analysis with the fitted simplified form of $g(\xi)$ shown in Fig. 4 for $Wi = 5, 10, 15, 25$, and 50 . The solid line $y = 0.12 + 5.94x$ is the least square fit.

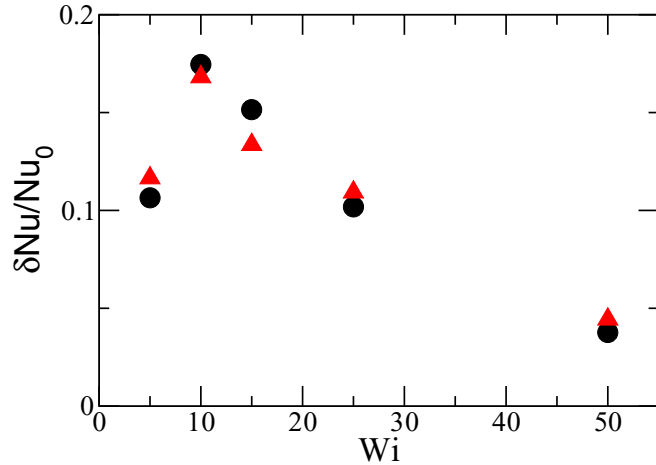


FIG. 6. Comparison of the DNS results of the relative change in Nu, $\delta\text{Nu}/\text{Nu}_0$ (circles), against the results obtained using our present analysis as explained in the text (triangles).

and the relative enhancement in Nu increases monotonically with Wi as obtained by the generalized PBP theory.

Using the fitted linear relation (see Fig. 5) and the DNS results of ε_u we can obtain $\delta\text{Nu}/\text{Nu}_0$ from $(\delta\text{Nu}/\text{Nu}_0)_{\text{PBP}}$ and make a direct comparison of the results so obtained with the DNS results. The good agreement found (see Fig. 6) is another verification of the goodness of the linear fit in Fig. 5.

IV. CONCLUSIONS

Using DNS we have found that polymers start to affect turbulent RB convection and enhance the heat flux when Wi is greater than 2. For smaller Wi, polymer stretching is negligible. As Wi is increased, the amount of heat flux enhancement first increases but when Wi is beyond around 10, the heat flux enhancement decreases when Wi is further increased. This nonmonotonic behavior of heat flux enhancement is a combined result of decrease in the viscous energy dissipation rate ε_u and the increase in the energy dissipation rate due to polymers ε_p as Wi is increased. The decrease in ε_u with Wi,

which has already been observed in DNS study of the ultimate regime using periodic boundary conditions [2], is due to the increase of the Lumley scale l_L with Wi, whereas ε_p increases with Wi as a result of the increase in polymer stretching. We have analyzed the relative change in heat flux when ε_u is held fixed, $\delta\text{Nu}/\text{Nu}_{\varepsilon_u \text{ fixed}}$, using the generalized PBP boundary layer theory supplemented by a space-dependent effective viscosity, which represents the effect of polymer stretching. To calculate theoretically the effective viscosity profile, one would need to estimate the amount of polymer stretching in the bulk of the system and its nonlinear coupling with the boundary layers. Such a theoretical development is outside the scope of the present paper. Instead we have used the DNS data to compute the effective viscosity and taken it as an external input for the generalized PBP analysis. Our generalized PBP analysis has demonstrated that heat flux enhancement occurs as polymers are stretched mostly in the bulk of the system and the amount of heat enhancement increases with Wi. We have further confirmed that the values of $\delta\text{Nu}/\text{Nu}_{\varepsilon_u \text{ fixed}}$ are well fitted by a linear function of $(\delta\text{Nu}/\text{Nu}_0)_{\text{PBP}}$ obtained in the generalized PBP analysis. Together with the DNS results of ε_u , we are then able to obtain the nonmonotonic heat flux enhancement with Wi. Our analysis thus provides a physical way to understand the DNS results.

Our theoretical approach has the advantage of being quantitative and based on the well-established definition of effective viscosity and momentum balance near the boundary (the Prandtl-Blasius equations). In comparison to the well-known problem of drag reduction by polymers in wall-bounded turbulence, the effect of polymers in turbulent RB convection can be developed using the well-established approach for boundary layer dynamics (with the caveats previously highlighted) and we remark that this is an important point to be exploited in the future. It remains an open question what may happen for large Ra at which Nu is dominant from contribution to ε_u from the bulk flow and the physical ground for using the boundary layer approximation breaks down.

ACKNOWLEDGMENTS

The work of ESCC was supported by the Hong Kong Research Grants Council under Grant No. CUHK-400311.

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